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# COST – EFFECTIVE SOLUTIONS FOR SEWAGE TREATMENT IN DEVELOPING COUNTRIES

THE CASE OF BRAZIL

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BRAZIL

Introduction

The CEPT Experience

The UASB Experience

Discussion

#### Introduction

The CEPT Experience

The UASE Experience

Discussion

## Introduction

- Less than 55% of the urban population of Brazil has public sewers, and less than 20% of the wastewater is treated.

- The challenge: which are the most efficient and costeffective levels of treatment? Which processes provide sustainability in a developing country such as Brazil?

## Introduction

Special attention has been given to the so called low-cost treatment:

- Chemical Enhanced Primary Treatment (CEPT);
- Upflow Anaerobic Sludge Blanket Reactors (UASB);
- Chemical Sludge Stabilization (CSS).

Introduction

The CEPT Experience

The UASE Experience

Discussion

### A + 100 years old process

It was used in USA, until 1930s; it fell into disfavor due to:

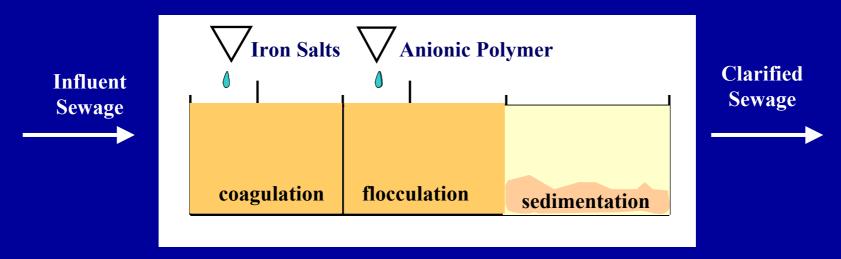
- The required high application of metal salts;
- Consequent high chemical sludge generation;
- Advent of the activated sludge process.

#### Nowadays, the CEPT process found its place again:

- Recent offer of less costly chemicals;
- Low dose chemical coagulation, new polymers.

### **Process Description**

CEPT is a wastewater treatment technology based on suspended solids removal by physical-chemical processes of coagulation, flocculation and sedimentation.



- BOD removal up to 50%; TSS removal up to 80%;
- Great economy in investment costs.

### Results obtained in Brazil





The difference between such results, may be explained by both plants being operated well under design flow and having part of the flow diverted from two different polluted rivers

| Month (*) - | BOD removal (%) |             | TSS removal (%) |             |
|-------------|-----------------|-------------|-----------------|-------------|
|             | Pavuna STP      | Sarapuí STP | Pavuna STP      | Sarapuí STP |
| June        | 63,3            | -           | 78,5            | 67,1        |
| July        | 69,9            | 42,7        | 62,9            | 65,0        |
| Aug.        | 60,8            | 39,0        | 65,4            | 82,1        |
| Sept.       | 69,6            | 42,1        | 70,4            | 85,1        |
| Oct.        | 59,7            | 41,1        | 55,3            | 75,1        |
| Nov.        | 63,2            | 43,0        | 52,6            | 65,1        |
| Dec.        | 59,0            | -           | 67,7            | 65,0        |

### **Sludge Increase**

- Sludge generation is increased in the CEPT concept;
- Increase costs in sludge conditioning, stabilization and drying.

Conventional activated sludge preceded by CEPT process (30mg/l FeCL<sub>3</sub> dose)



Conventional activated sludge preceded by conventional primary clarifiers



Hyperion, Los Angeles (increase of 24%)

## **Chemical Sludge**

In Brazil, the higher costs due to sludge augmentation have been counterbalanced by choosing Chemical Sludge Stabilization (CSS) instead of the classic anaerobic digestion: Pavuna, Sarapuí, Goiânia, Virgem Santa, Guapimirim, Lavapés STP.

#### The case of Goiânia STP:

| Sludge Treatment          | Initial Stage: Primary Treatment CEPT | Final Stage: Secondary Treatment CEPT + Activated Sludge |
|---------------------------|---------------------------------------|----------------------------------------------------------|
| Anaerobic Digestion       | R\$ 18 x 10 <sup>6</sup>              | R\$ 63 x 10 <sup>6</sup>                                 |
| Chemical Stabilization    | R\$ 10 x 10 <sup>6</sup>              | R\$ 47 x 10 <sup>6</sup>                                 |
| Economy                   | 44%                                   | 25%                                                      |
| ( * ) Database: year 1999 |                                       |                                                          |

Introduction

The CEPT Experience

The UASB Experience

Discussion

#### The main characteristics

High sludge age (usually over 30 days)



Smaller amount of excess sludge produced

Low hydraulic detention time



**Lower construction costs** 

#### The main characteristics

- Compact system, using a small surface area;
- Practically no equipment in the anaerobic vessel, with low construction and operational costs;
- Very low energy consumption;
- Low excess sludge produced;
- The excess sludge has a good concentration, with good drying characteristics.

### The main disadvantages

- High potential for H2S generation; bad odors?
- Low capacity of receiving toxic loads;
- Low start-up; inoculation needed;
- Effluent: below legal standards;
- Limited efficiency: 45-70% COD; 55-75% BOD;
- < 1log FC; 0% N, P.</p>

#### **UASBs** in Brazil

- Onças STP, Belo Horizonte, MG: 3,0 m<sup>3</sup>/s (design phase)
- Atuba Sul STP, Curitiba, PR: 1,5 m³/s (operational)
- Sta. Quitéria STP, Curitiba, PR: 0,6 m³/s (operational)
- Piracicamirim STP, São Paulo, SP: 0,4 m³/s (operational)
  - BOD Efficiency: between 55 and 75%
  - **COD** Efficiency: between 50 and 70%

## Legislation

- UASB effluent always above 60 mgBOD/l, up to 120;
- Above legal limits;
- 30 to 60 mg/l are required according to different State legislation.

Research Program on feasible technologies for UASB post-treatment

## **UASB + Post-treatment: Research Program**

| Process                                     | Discritption                                       | Average Design                 |  |  |
|---------------------------------------------|----------------------------------------------------|--------------------------------|--|--|
| Trickling Filter                            | Gravel media                                       | 0,75 BOD/m <sup>3</sup> d      |  |  |
| Aerated Submersed Filter                    | Gravel media                                       | 0,85 BOD/m <sup>3</sup> d      |  |  |
| Acidica Gubinersea i liter                  | PVC modules or plastic media                       | 1,6 BOD/m <sup>3</sup> d       |  |  |
|                                             |                                                    | 40 mg/l                        |  |  |
| Dissolved Air Flotation                     | With FeCl <sub>3</sub> coagulation and floculation | 20 minutes                     |  |  |
|                                             |                                                    | 30 - 60 - 90 s <sup>-1</sup> G |  |  |
| Aerated Ponds                               | Machanical aerators                                | 2 days detention time          |  |  |
| Acrated Folias                              | Sedimentation ponds                                | 1 day detention time           |  |  |
| Activated Sludge                            | Plug flow aerated tanks                            | 4 days sludge age              |  |  |
| ( * ) for temperatures between 20 and 26 °C |                                                    |                                |  |  |

## **UASB Design Criteria**

| Criteria                                       | Value for avarege flow                        |
|------------------------------------------------|-----------------------------------------------|
| Hidraulic volumetric load                      | < 4,0 m <sup>3</sup> /m <sup>2</sup> .d       |
| Hidraulic detention time                       | 6,0 - 9,0 h                                   |
| Upflow velocity                                | 0,5 - 0,7 m/h                                 |
| Overflow rate in the clarifier zone            | 14,4 - 19,2 m <sup>3</sup> /m <sup>2</sup> .d |
| Hydraulic detention time in the clarifier zone | 1,5 - 2,0 h                                   |
| Solids generation                              | 0,1 - 0,2 Kg TSS/Kg influent COD              |
| Excess sludge concentration                    | 2,0 - 5,0 %                                   |
| Sludge specific weight                         | 1020 - 1040 Kg TSS/m <sup>3</sup>             |
| ( * ) for temperatures betw een 20 and 26 °C   |                                               |

Introduction

The CEPT Experience

The UASB Experience

Discussion

#### **CEPT** as a Pre-Treatment Process

When applying any chemical process, one must be aware of the many disadvantages that chemical products have:

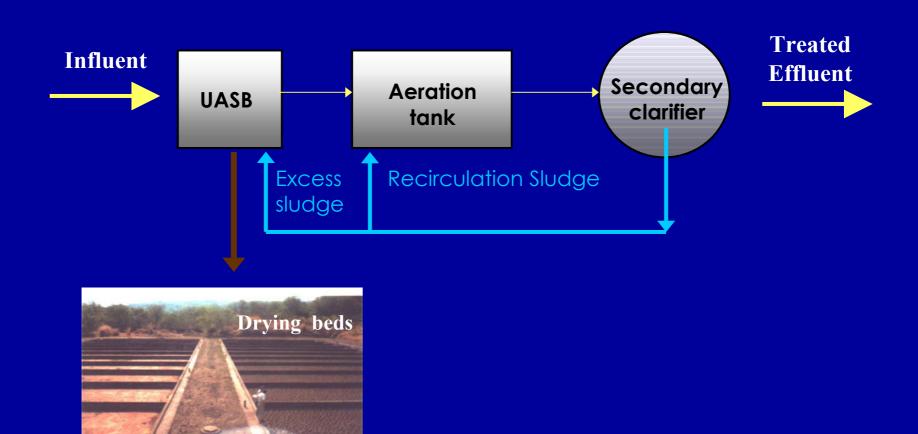
- Acquisition
- Storage
- Handling
- Safety
- Costs

#### **CEPT** as a Pre-Treatment Process and its Costs

#### The case of Goiânia STP:

| Treatment Pattern                                                                                         | Initial Stage<br>(R\$ x 10 <sup>6</sup> ) | Final Stage<br>(R\$ x 10 <sup>6</sup> ) | Final Stage<br>(R\$ x 10 <sup>6</sup> ) |
|-----------------------------------------------------------------------------------------------------------|-------------------------------------------|-----------------------------------------|-----------------------------------------|
| Conventional Primary + Activated Sludge +     Anaerobic Digestion                                         | 17,1                                      | 56,8                                    | 60,7                                    |
| 2. CEPT + Activated Sludge + Anaerobic Digesti                                                            | on 18,7                                   | 45,6                                    | 55,8                                    |
| 3. CEPT + Activated Sludge + CSS                                                                          | 10,5                                      | 37,5                                    | 55,6                                    |
| 4. CEPT + Anaerobic Digestion (IS) and Conventional Primary + Activated Sludge + Anaerobic Digestion (FS) | 18,9                                      | 51,6                                    | 63,4                                    |

#### **UASB** reactors as Pre-Treatment units



#### **UASB** reactors as Pre-Treatment units

- Double the BOD or COD removal rates (as compared to conventional primary units);
- Lower volume of sludge produced;
- Construction and operation costs are lower;
- The plant may be constructed in stages: first the UASB, later the pos-treatment;
- Costs of secondary treatment units are reduced by about half;

#### **UASB** reactors as Pre-Treatment units

- In the activated sludge process following an UASB reactor, the energy is cut to 45 to 55% of the conventional system without nitrification, and up to 65 to 75% with nitrification;
- The cost of UASB + aerobic treatment < 80% of the cost of a conventional secondary treatment;
- Sludge production is lower and the excess can be returned to the UASB reactor;
- The final excess sludge is well digested and has good drying proprieties.

Introduction

The CEPT Experience

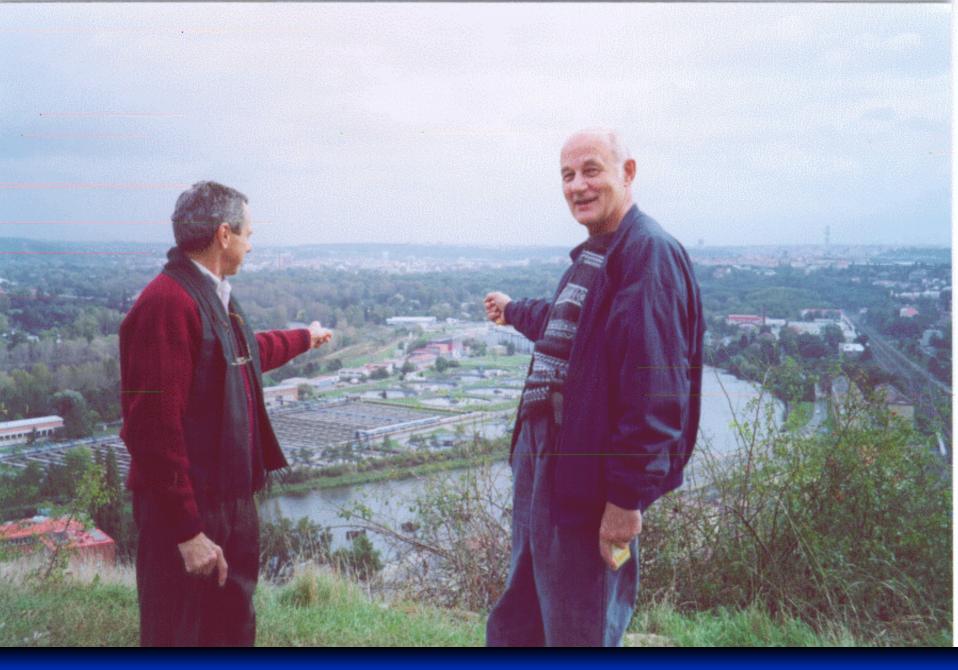
The UASB Experience

Discussion

## Conclusion

#### **CEPT or UASB = GREAT BENEFITS**

- They reduce the size, the investment and the operational cost of secondary treatment;
- They can be implemented in steps of treatment and are competitive to other technologies;
- They prove to be feasible for developing countries, where construction costs are always a limiting factor for sewage treatment expansion.



# PRAGUE STP

